PHOSPHORUS REMOVAL TECHNOLOGIES SUMMARY

TABLE 2.1

Process/ Technology # Name 1. EBPR (AO)	Process/Tech Description Enhanced Biological Phosphorus Removal (EBPR)	Facilities/Chemicals Required Construction/Creation of Anaerobic zone at beginning of the activated skudge process • no chemicals required	Effluent Phos. Limits achievable 0.8 – 1.2 mg/l	Performance History/ Number of Installations Established technology, growing number of installations	Process/ Biosolids Impacts Slight increase in sludge production	Estimated Construction Costs ⁽¹⁾ \$2,500,000	Ability to PO4 Limits of:		
							1.0 X	.36	
2. Primary Chemical Precipitation	Metal Salt addition upstream of Primary Clariflers	Cherrical Storage and Feeding Equipment Building Addition Primary clarifier improvements Sludge pumping improvements	0.6 – 1.0 mg/l	Weil established technology, numerous installations	Moderate increase in studge production	\$655,000	x		
3. Secondary Chemical Precipitation	Metal Salt addition upstream of Secondary Clarifiers	Chemical Storage and Feeding Equipment Required	0.5 - 0.9 mg/l	Well established technology, numerous installations	Small increase in sludge production	\$1,130,000	x		
4. Multi Point Chemical Addition	Metal Satt addition upstream of both Primary Clarifiers and Secondary Clarifiers	Chemical Storage and Feeding Equipment Required Building Addition Primary clarifier improvements Studge pumping improvements	0.4 0.8 mg/l	Well established technology, numerous installations	Larger increase in sludge production	\$1,600,000	x		
5. EBPR w/ Chemical Addition	EBPR with secondary Chemical Addition	Construction/Creation of Anaerobic zone at beginning of the activated sludge process Chemical Storage and Feed Equipment Sludge pumping improvements	0.3 - 0.6 mg/	Established technology, many installations	Larger increase in studge production	\$3,630,000	x		
6. EBPR w/ Chemical Addition & Filtration	EBPR with secondary Chemical Addition and Tertiary disc Filtration	Construction/Creation of Anaerobic zone Chemical Storage and Feed Equipment Effluent Disc Filters required New Ballding	0.1 – 0.3 mg/i	Established technology, many installations	Larger increase in skudge production	\$6,630,000		×	
7. Multi Point Chemical Addition w/ Filtration	Multi Point Chemical Addition and Tertiary Filtration	Chemical Storage and Feed Equipment Effluent disc Filters required New Building	0.1 — 0.3 mg/ī	Established technology, many installations	Large increase in sludge production	\$4,600,000		x	
8. Tertiary Clarification w/ two stage Filtration	Tertiary Solids Contact Clartfiers for Chemical Precipitation, followed by two stage Filtration	Construction of Tertiary Solids Contact Clarifiers Effluent Filters required New Building	0.03 - 0.1 mg/l	Established wastewater treatment technology, with many wastewater installations	Moderate increase in studge production	\$7,455,000			x
9. MBR w/ Chamical Addition	Membrane Biological Reactor w/ Multi Point Chemical Addition	Construction of Membrane Biological Reactor Chemical Storage and Feeding Equipment	0.01 <u>– 0.1</u> mg/l	Emerging technology, many installations	Large increase in studge production	\$10,500,000			x
10. Terüary Bailasted Floc	Baltasted Clarification Process	CoMag® (Magnetite Weighted) or Actific® (Sand Weighted) proprietary process equipment Chemical Feed Systems	0.01 – 0.1 mg/l	New and Emerging technology being piloted, no installations for CoMag, few for Actilio	Potentially small increase in sludge production	\$6,530,000			x
11. Tertiary Membrane w/ Chemical Addition	Multi Point Chemical Addition followed by Tertiary Membrane Microfiltration	Construction of in- tank Membrane Microfiltration equip. Chemical Storage and Feed Equipment - Sludge pumping improvements	0.01 — 0.05 mg/l	New and Emerging technology being piloted, few installations	Potentially large increase in sludge production	\$8,855,000			x

Notes: 1) Capital Costs are for PO₆ Usit p WWTP. d facili c. Costs have not be

